



D2.3

CO₂ capture by selected ashes and LCA

Grant Agreement No.	101058162
Project start date	01.06.2022
Duration of the project	48 months
Deliverable number	D2.3
Deliverable leader	ZAG
Dissemination level (PU, SEN, CI)	PU
Status	v0.4
Submission date	31.05.2024
Author, organisation, e-mail	Sara Tominc, ZAG, sara.tominc@zag.si
Modification control	

VERSION	DATE	DESCRIPTION AND COMMENTS	AUTHOR
0.1	19.02.2024	Creation of the document and description of the methodology	Sara Tominc (ZAG)
0.2	29.04.2024	Results	Sara Tominc (ZAG)
0.3	8.05.2024	Review of the document	Vilma Ducman (ZAG) Wolfgang Wisniewski (ZAG)
0.4	23.05.2024	Finalising the document	Sara Tominc (ZAG)



**Funded by
the European Union**

List of contributors:

- Sara Tominc (ZAG)
- Vilma Ducman (ZAG)
- Wolfgang Wisniewski (ZAG)
- Stijn Matthys (UGhent)
- Beibel Sun (UGhent)
- Marie-Laure Heyndrickx (UGhent)
- Jolien Smeets (Orbix)
- Dirk Van Machelen (Orbix)
- Guang Ye (TUDelft)
- Boyu Chen (TUDelft)
- Abdellah Hussein (TUDelft)



**Funded by
the European Union**

Table of Contents

Objective.....	1
Introduction.....	2
1. Methodology	4
1.1. Scope	4
1.2. Characterization	4
1.3. Mineral carbonation.....	5
1.4. Analysis with a pressure calcimeter.....	6
1.5. Thermogravimetric analysis (TGA)	7
2. Results.....	7
2.1. Slovenia	8
2.2. Croatia	9
2.3. Denmark	10
2.4. Finland.....	11
2.5. The Netherlands	11
2.6. Belgium.....	11
3. RESULTS FOR LCA	12
4. SUMMARY AND CONCLUSIONS.....	14
References	15
Appendix.....	18

Table of Figures

Figure 1: Methodology for evaluating the CO ₂ sequestration potential of waste ashes. 4	
Figure 2: Thermogravimetric analysis of selected sample a) #SI.WA.BA.1 with the maximum CO ₂ content after 14 days of carbonation in the temperature range from 550 to 950 °C and b) #SI.CC.FA.4 after 28 days of carbonation in the temperature range from 400 to 700 °C.	9

Table of Tables

Table 1: TGA and calcimetric measurements for wood and co-combustion ashes from Slovenia.	8
Table 2: TGA and calcimetric measurements for WBA and SSA from Croatia.	9
Table 3: TGA and calcimetric measurements for MSWI ashes and SSA from Denmark.	10
Table 4: TGA and calcimetric measurements for co-combustion ashes from Finland.	11



**Funded by
the European Union**

Table 5: TGA and calcimetric measurements for biomass ashes from the Netherlands.	11
Table 6: TGA and calcimetric measurements for the ashes received from Orbix.	12
Table 7: TGA and calcimetric measurements for co-combustion and MSWI ashes from Belgium.	12
Table 8: Maximum CO ₂ sequestration capacity for each analyzed ash.	13

Abbreviations

CCUS	carbon capture, utilization and storage
Gt	gigaton
LCA	life cycle assessment
L/S	liquid to solid
MSWI-BA	municipal solid waste incineration bottom ash
MSWI-FA	municipal solid waste incineration fly ash
ppm	parts per million
RH	relative humidity
SSA	sewage sludge ash
WB-BA	wood biomass bottom ash
WB-FA	wood biomass fly ash

Objective

The main objective of this deliverable, as defined in Task 2.3 of the AshCycle project, is to assess the carbon storage capacity (sequestration potential) of the ashes considered in this project, i.e. sewage sludge ash (SSA), municipal solid waste incineration bottom/fly ash (MSWI-BA and MSWI-FA), and wood biomass bottom/fly ash (WB-BA and WB-FA).

Ashes containing a high amount of free CaO represent a potential for binding CO₂ into the stable form of carbonates. The amount of free CaO depends on both the type of fuel and the combustion process. Accelerated carbonation makes the ash more stable and therefore easier to reuse. However, various parameters can significantly influence the process, e.g. particle size, RH, temperature, exposure time and CO₂ concentration. Carbon sequestration is also investigated with regard to carbstone concrete products (Task 4.3, cement-free concrete curing in a CO₂ chamber). Such a process could become part of incineration plants and offers two advantages: stabilised ash and lower CO₂ emissions, which can also be achieved by a long-term use of the ash. The results of the potential for temporary carbon storage are assessed as part of the life cycle assessment (global warming potential indicator).



**Funded by
the European Union**

Introduction

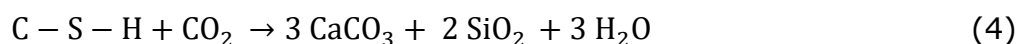
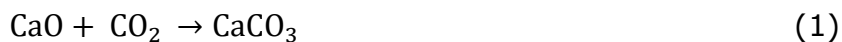
The concentration of CO₂ in the atmosphere has been below 300 ppm for thousands of years [1]. CO₂ emissions from fossil fuels play an important role in the accumulation of CO₂ in the atmosphere, as the burning of fossil fuels, cement production and other industrial processes release more than 36 Gt of CO₂ worldwide every year [2]. The CO₂ concentration has risen steadily since the beginning of the industrial revolution when it was around 280 ppm [3]. In 2014, the CO₂ concentration in the atmosphere exceeded 400 ppm for the first time and is currently increasing by around 1% per year [4,5]. In 2022, the CO₂ concentration in the atmosphere exceeded 420 ppm, and in May 2023, CO₂ emissions reached a record level of 424 ppm [5]. The increase in CO₂ concentration in the atmosphere leads to global warming and consequently to climate changes such as a rise in the average global temperature, increasing air pollution, changes in the pattern and amount of rain and snow fall, changes in relative humidity, the melting of ice in polar regions, a rise of the average sea level, a decline in agricultural production and the extinction of fauna and flora [6,7].

Due to climate change and environmental degradation in Europe and the rest of the world, there is an urgent need to reduce CO₂ and greenhouse gas emissions. To overcome these challenges, the European Commission adopted the European Green Deal in 2020, committing the European Union to become climate neutral by 2050 [8]. The European Union's initiatives are aimed at various sectors, including the construction industry, transport and renewable energies. In the first phase, net greenhouse gas emissions are expected to be reduced by at least 55% by 2030 compared to 1990 levels [8]. In the technological segment related to construction, several technologies are currently being developed or improved that will mainly contribute to the first phase. These include various recycling methods and industrial symbioses such as alkali-activation and carbonation as well as carbon capture, utilization, and storage (CCUS) technologies. CCUS is an extremely hot topic in EU climate policy because of its potential role in avoiding CO₂ emissions that are difficult to reduce. Although CCUS technologies have been in use since the 1970s, their widespread implementation is still challenged by a range of factors, including political inertia, high costs and their relative novelty in the public discourse [9]. Despite the current energy and cost-intensive technologies for carbon capture and storage, CO₂ mineral sequestration represents a straightforward approach. It primarily involves the reaction of CO₂ with alkaline materials, composed of Ca and Mg rich (hydr)-oxides and silicates, leading to the formation of solid carbonate products and their subsequent storage [2], [10–12]. The exothermic nature of the mineral carbonation reaction can potentially compensate for the energy consumption in CO₂ sequestration and achieve low costs [13,14].

Carbonation is a natural chemical reaction process in which CO₂ initially dissolves in water. As directly binding molecular CO₂ to CaO is very slow (Equation (1)), it dissociates, and reacts with Ca(OH)₂ (also with calcium silicate hydrate (C-S-H), calcium aluminate hydrate (CAH), etc.) to form CaCO₃ (Equations (2)-(4)). The main product (CaCO₃) is thermodynamically stable, meaning it is unlikely that CO₂ will be released under normal conditions [6,11,15].



**Funded by
the European Union**



While spontaneous carbonation with atmospheric CO_2 (0.04%) is generally very slow, carbonation can be accelerated by an increased CO_2 concentration or pressure [11, 16,17]. Accelerated carbonation leads to a higher carbonation rate, which is influenced by the carbonation conditions such as the particle size of the selected material, the relative humidity (RH), the liquid to solid (L/S) ratio, the temperature, the contact time, the pressure and the CO_2 concentration [6,18–20]. Although the accelerated carbonation of industrial residues has been the subject of numerous research studies over the last decade [10,13,21–24], there is still a lack of systematic evaluation for the influence of the relevant operating parameters in the scientific literature. In this context, it is essential to find optimal conditions that maximize the potential of the selected material as a carbon sink. In order to mitigate climate change fast enough, accelerated carbonation is highly favourable over natural carbonation.

Particle morphology seems to be important as CO_2 uptake increases when particle size is reduced due to a larger specific area exposed to CO_2 [6,19,25–27]. Water is essential for the reaction kinetics of carbonation, while the CO_2 concentration in the gas has a smaller influence. Some studies have shown that the reaction rate and the conversion rate of Ca(OH)_2 increase with increasing RH [18,28,29], where the optimum RH for the carbonation rate is between 60 and 80% [7,30]. Excess moisture can saturate the material and lower its permeability, which can limit the movement of CO_2 into the material and the depth at which carbonation can occur [31]. Increasing the temperature accelerates the reaction kinetics. Carbonates form quickly on the surface, reaching saturation and limiting the further penetration of CO_2 into the material [32].

Waste incineration is steadily increasing throughout Europe, but there are environmental concerns regarding solid residues which are usually landfilled [33]. There are several options for using the received or pre-treated ash, of which CO_2 sequestration by accelerated mineral carbonation is a promising carbon capture and storage technology. However, not much is known about the sequestration potential of waste ashes. The main problem, which is important for wide utilization, is to keep the properties of the heterogeneous ash constant [34]. Ashes with a high content of Ca and Mg compounds, especially ashes from wood biomass, are promising candidates for sequestration [18,34,35]. The high availability of ash as a by-product of solid fuel combustion is therefore an additional advantage. Recently, Tominc and Ducman [18] have shown that a high CO_2 sequestration capacity for WBA can be achieved by a semi-dry mineral carbonation process.

1. Methodology

As part of the AshCycle project, we analysed ashes from different incineration plants and determined its potential for carbon sequestration [18], as visualized in Figure 1. The methodology was first applied to eight different ashes and then improved by optimising the carbonation conditions, as not all ashes are equally suitable for CO₂ sequestration.

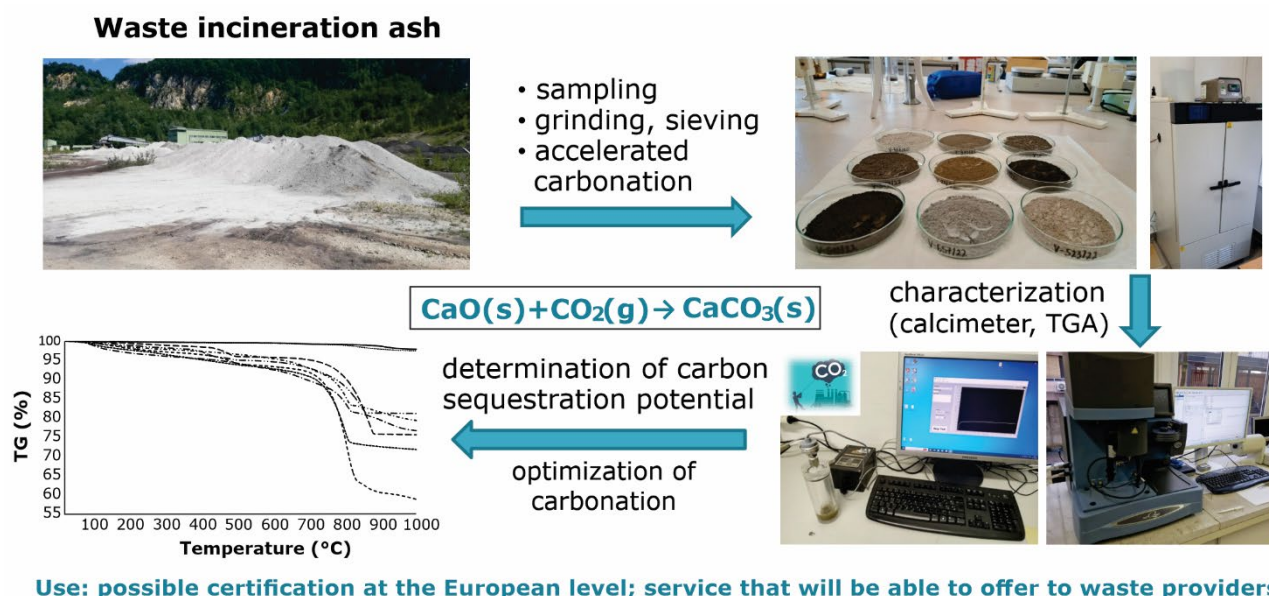


Figure 1: Methodology for evaluating the CO₂ sequestration potential of waste ashes.

1.1. Scope

The methodology was established to determine the carbon sequestration potential of the ashes considered in this project. The evaluation includes sample preparation, characterization and analysis with a pressure calcimeter and a thermogravimetric analyzer.

As a tool, this methodology can also be used to evaluate other waste materials and support the development of construction materials based on the solidification of the material. This enables the long-term use of waste materials and contributes to the reduction of global CO₂ emissions by reducing the need for cement.

1.2. Characterization

1.2.1. Sampling

All samples were homogenized by quartering, packed in a PVC bag, and stored in a plastic container.

1.2.2. Chemical analysis (XRF)

The ashes were sieved below 125 μm for chemical analyses, dried at 105 °C, and heated at 950 °C to determine their loss on ignition (LOI); a fused bead was then prepared with a mixture of ash and flux (50% lithium tetraborate/50% lithium metaborate) in a 1:10 ratio (0.947 g: 9.47 g) and heated at 1100 °C. The standard deviation of repeatability for LOI is 0.04 mass% according to the standard EN 196-2:2013 [36]. The chemical composition of the ashes was then determined using a ARL PERFORM'X Wavelength Dispersive X-Ray Fluorescence Spectrometer (WDXRF; Thermo Fischer Scientific Inc., Ecublens, Switzerland) with an Rh-target X-ray tube and the UniQuant 5 software (Thermo Fisher Scientific Inc., Waltham, MA, USA). Two measurements were performed for each ash. The average values are listed in the Appendix.

1.2.3. Mineralogical analysis (XRD)

The ashes were sieved below 63 μm and placed in 27 mm holders (in diameter) for mineralogical analyzes performed before and after CO₂ exposure with X-ray diffraction (XRD; Empyrean X-ray Diffractometer, Cu X-ray source; PANalytical, Almelo, The Netherlands) in 0.013° steps from angles of 4–70° under clean room conditions, using the external standard corundum NIST SRM 676a. The mineral content was evaluated using the PANalytical X'Pert High Score Plus diffraction software v.4.8.

1.3. Mineral carbonation

1.3.1. Sample preparation

The obtained ash was first ground and sieved to a particle size of less than 125 μm . Then 20 g of each were placed in a petri dish and exposed in a closed CO₂ carbonation chamber.

1.3.2. Carbonation conditions

Selected ashes were first tested at a RH of 50-55% at a temperature of 20 °C and 4 \pm 0.1 vol% CO₂. Then the ashes were tested at an increased RH of 80-85% at a temperature of 20 °C and 4 \pm 0.1 vol% CO₂. Samples were taken after 1, 7, 14, 21 and 28 days. To optimize carbonation conditions, selected ashes were treated with 20 \pm 0.1 vol% CO₂ for 3 days and with 4 \pm 0.1 vol% CO₂ for at least 7 days at a RH of 80% and a temperature of 40 °C.

1.3.3. Determination of the constant mass

Carbonation was complete when a constant mass was reached. The mass is constant if the difference between two weighings is less than 0.1 g.

1.4. Analysis with a pressure calcimeter

1.4.1. General

The obtained and carbonated ashes were analysed with the pressure calcimeter (OFITE Calcimeter, OFI Testing Equipment Inc., Houston, TX, USA, according to ASTM D 4373) with an analytical error of <5%.

The OFITE calcimeter is used to determine the amount of CaCO_3 and Ca/Mg carbonate (dolomite) in a sample. CaCO_3 reacts with 10% HCl in a closed reaction cell and forms CaCl_2 , CO_2 and H_2O . The pressure of the released CO_2 is measured with a manometer. The calcimeter is calibrated by reacting HCl with pure CaCO_3 before the actual measurements.

1.4.2. Test procedure

Each sample was ground and sieved below 125 μm and dried in an oven at 105 °C for 24 h. Then 1.0 ± 0.01 g of the sample was weighed and added to the reaction cell. The acid cup was filled with 20 mL of 10% HCl and carefully placed in the reaction cell. The vent valve was opened until the pressure was zero, then the vent valve was firmly closed to start the measurement. The reaction cell was swirled for one minute and then held until the reaction was complete, i.e. after 40 minutes. The percentage of CaCO_3 and dolomite in the sample was calculated using the software.

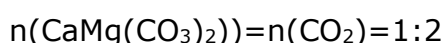
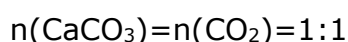
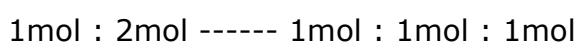
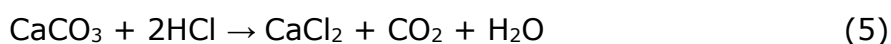
1.4.3. Construction of the calibration curve

The volume of a calcimeter reaction cell determines the relationship between the pressure increase and the amount of released CO_2 . This relationship is constant for a given reaction cell. The calibration is required before the first test. The software uses a calibration curve to convert the released pressure into a percentage of CaCO_3 .

Five sets of CaCO_3 samples with the following masses were used for calibration: 0.2 g, 0.4 g, 0.6 g, 0.8 g, 1.0 g. All samples were weighed with a margin of error of ± 0.01 g. At the end of the calibration, the software displayed the r^2 value as shown in Figure A1.

1.4.4. Calculations

The calculations for the amount of released CO_2 were based on the stoichiometry.



**Funded by
the European Union**

$$M(\text{CaMg}(\text{CO}_3)_2) = 184.4008 \text{ g/mol}$$

1 mol of $\text{CaMg}(\text{CO}_3)_2$ releases 88.02 g of CO_2 .

1.5. Thermogravimetric analysis (TGA)

1.5.1. General

A thermogravimetric analysis (TGA) was performed on carbonated ashes using a TGA Q5000IR thermal analyzer (TA Instruments, New Castle, Delaware, USA).

The TGA measures the mass change of a sample when it is subjected to a temperature program in a controlled atmosphere [37]. Due to possible hydration reactions contributing to the weight gain, TGA is a suitable method to quantify the increase in CaCO_3 content during carbonation and provides quantitative information on the extent of carbonation [16,19].

1.5.2. Test procedure

TGA was performed from 25 to 1000 °C, with a heating rate of 10 K min⁻¹. Prior to the measurements, the ashes were dried at 105 °C and sieved to a grain size below 63 µm. To prevent oxidation during the measurement, the sample chamber was filled with N_2 with a flow rate of 25 mL min⁻¹. Ash batches were placed in 100 µL Al_2O_3 crucibles.

Using the TGA, we measured the weight loss in the temperature range of decomposition of the carbonate mineral (between 550-950 °C), with an analytical error of <1 %. The results were analyzed using TA Universal Analysis 2000 v.4.5A (TA Instruments, New Castle, Delaware, USA).

2. Results

The results of the assessment of the sequestration potential of the individual ashes are given separately for each country of origin. The ashes were given a systematic name: #country.type.number. Details of the selected ashes were provided in Deliverable 2.1: Ash characterization and categorization.

The ashes were exposed to accelerated carbonation conditions in a closed carbonation chamber at elevated CO_2 concentration and different humidities and temperatures until maximum CO_2 uptake. Maximum CO_2 uptake was achieved at room temperature and elevated humidity (80%) after 28 days of carbonation. By optimizing the carbonation conditions, maximum CO_2 uptake was achieved after 7-14 days of carbonation at elevated temperature (40 °C) and humidity (80%) for the selected ashes.

The highest sequestration potential was found for ashes from wood biomass from Slovenia, Croatia and the Netherlands as well as from co-combustion of wood waste and paper sludge from Slovenia (#SI.CC.MA.2), while SSA or MSWI ashes showed a lower sequestration potential.



**Funded by
the European Union**

2.1. Slovenia

In Table 1 CO₂ content (in wt%) according to TGA and measured with a pressure calcimeter is compared. The maximum CO₂ content of both methods in each ash is shown in bold. As we can see, the results in ashes from wood biomass are very comparable, in the case of ash #SI.WA.BA.1 the difference between the determination by TGA and the calcimeter is 1.4%. As shown in Figure 2a, the weight loss in the temperature range of decomposition of carbonate minerals was between 550-950 °C, while Figure 2b shows that we detect different phases in this temperature range, as the difference between the calcimetric measurement and TGA is up to 22.5%. If we narrow down the weight loss in the temperature range of 400-700 °C, we obtain a comparable result to the calcimetric measurement (9.7 wt%).

Due to these differences between the TGA and the calcimetric determination, the CO₂ sequestration capacity of all ashes was quantified for further LCA calculations using the calcimetric method. With TGA, it is necessary to limit the temperature range for each ash individually. Of the Slovenian ashes, the WB-BA and the co-combustion mixed ash achieved the highest sequestration potential with a CO₂ content of 30.2 wt% (#SI.WA.BA.1) and 27.6 wt% (SI.CC.MA.2).

Table 1: TGA and calcimetric measurements for wood and co-combustion ashes from Slovenia.

Sample ID	CO ₂ conc. (%)	T (°C)	RH (%)	Time (days)	TGA (weight losses-%)		Calculations (TGA)		Calculations (calcameter)		
					0-150 °C	550-950 °C	% dry matter	% CO ₂ /dry matter	% CaCO ₃	% Dolomite	% CO ₂
#SI.WA.FA.1	4	20	50	28	2.9	16.8	97.1	17.3	27.1	4.4	14.0
	4	20	80	28	2.4	17.6	97.6	18.0	33.0	3.1	16.0
	4	40	80	7	2.0	20.3	98.0	20.7	26.1	4.7	13.7
	4	40	80	14	2.0	21.0	98.0	21.5	27.0	5.2	14.4
#SI.WA.BA.1	4	20	50	28	3.2	26.1	96.8	26.9	52.0	0.5	23.1
	4	20	80	28	4.6	23.2	95.4	24.4	67.7	1.0	30.2
	4	40	80	7	2.8	27.9	97.2	28.7	66.7	1.1	29.8
	4	40	80	14	2.4	28.1	97.6	28.8	67.8	0.8	30.2
	20	40	80	3	3.4	26.8	96.6	27.7	58.1	0.7	25.8
#SI.CC.FA.2	4	20	50	28	1.6	11.8	98.4	12.0	13.8	0.3	6.2
	4	20	80	28	2.0	15.3	98.0	15.6	23.5	0.0	10.3
	4	40	80	7	1.3	12.7	98.7	12.9	19.2	0.3	8.6
	4	40	80	14	1.1	14.6	98.9	14.8	20.6	0.2	9.1
#SI.CC.MA.2	4	20	50	28	0.3	20.2	99.7	20.2	44.1	1.8	20.2
	4	20	80	28	1.3	28.8	98.7	29.2	59.9	1.6	27.1
	4	40	80	7	0.6	27.3	99.4	27.4	59.3	2.9	27.4
	4	40	80	14	1.5	27.0	98.5	27.4	61.3	1.3	27.6
	20	40	80	3	0.5	23.9	99.5	24.1	50.9	2.4	23.5
#SI.CC.FA.3	4	20	50	28	2.7	13.5	97.3	13.9	11.3	0.3	5.1
	4	20	80	28	2.9	15.8	97.1	16.3	22.1	0.0	9.7
	4	40	80	7	2.2	14.1	97.8	14.5	17.4	1.3	8.3

	4	40	80	14	2.2	15.8	97.8	16.2	19.1	0.7	8.7
	20	40	80	3	1.9	13.6	98.1	13.8	15.5	0.5	7.0
#SI.CC. BA.3	4	20	50	28	0.3	12.0	99.7	12.0	23.7	3.4	12.0
	4	20	80	28	0.7	13.7	99.3	13.8	30.5	1.3	14.0
	4	40	80	7	1.0	12.2	99.0	12.3	31.1	2.3	14.8
	4	40	80	14	1.0	12.7	99.0	12.8	34.4	1.7	15.9
#SI.CC. FA.4	4	20	50	28	2.5	31.5	97.5	32.3	19.5	2.6	9.8
#SI.CC. BA.4	4	20	50	28	1.6	11.4	98.4	11.5	29.4	6.2	15.9
	4	20	80	28	1.7	12.9	98.3	13.2	28.0	15.8	19.9
	4	40	80	7	1.9	10.8	98.1	11.0	26.5	17.8	20.2
	4	40	80	14	1.8	10.8	98.2	11.0	27.9	16.4	20.1

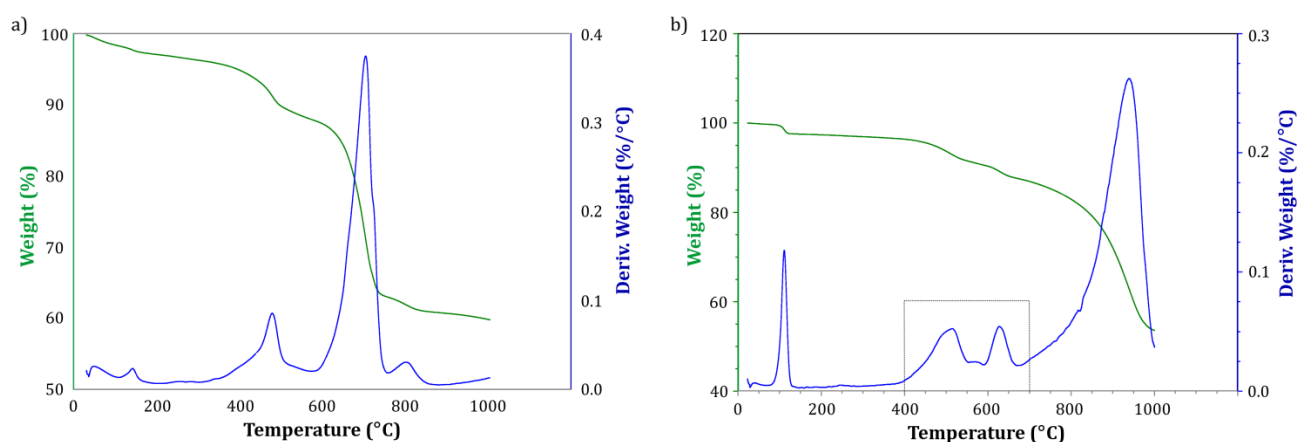


Figure 2: Thermogravimetric analysis of selected sample **a)** #SI.WA.BA.1 with the maximum CO₂ content after 14 days of carbonation in the temperature range from 550 to 950 °C and **b)** #SI.CC.FA.4 after 28 days of carbonation in the temperature range from 400 to 700 °C.

2.2. Croatia

Table 2 compares the CO₂ content according to TGA and measured with a pressure calcimeter in the ashes from Croatia. As we can see, the results for ashes from wood biomass are again very comparable, only for SSA there are higher deviations. Seven ashes from wood biomass showed a high CO₂ sequestration potential (with bound CO₂ above 20 wt%), with the highest value for #SI.WA.11 being 30.4 wt%.

Table 2: TGA and calcimetric measurements for WBA and SSA from Croatia.

Sample ID	CO ₂ conc. (%)	T (°C)	RH (%)	Time (days)	TGA (weight losses-%)		Calculations (TGA)		Calculations (calcimetric)		
					0-150 °C	550-950 °C	% dry matter	% CO ₂ /dry matter	% CaCO ₃	% Dolomite	% CO ₂
#HR. WA.1	4	20	50	28	2.4	19.5	97.6	19.9	38.4	0.3	17.0
	4	20	80	28	2.1	20.3	97.9	20.7	48.2	0.0	21.2
	4	40	80	7	2.4	21.1	97.6	21.6	47.0	1.7	21.5
	4	40	80	14	1.9	20.4	98.1	20.8	49.8	0.4	22.1
	20	40	80	3	2.0	19.0	98.0	19.4	46.3	0.6	20.6
#HR.	4	40	50	28	0.3	17.9	99.7	18.0	45.4	0.0	19.9

WA.2	4	20	80	28	0.9	24.0	99.1	24.2	61.9	0.0	27.2
#HR. WA.3	4	20	50	28	0.5	13.7	99.5	13.8	24.9	0.0	11.0
	4	20	80	28	0.6	22.4	99.4	22.5	45.1	0.0	19.8
#HR. WA.4	4	20	80	28	0.5	24.2	99.5	24.3	59.4	2.1	27.1
#HR. WA.6	4	20	80	28	0.7	16.9	99.3	17.0	35.8	3.1	17.2
#HR. WA.7	4	20	80	28	0.3	7.9	99.7	8.0	17.1	1.8	8.4
#HR. WA.8	4	20	80	28	0.7	23.8	99.3	23.9	53.2	2.6	24.6
#HR. WA.9	4	20	50	28	0.5	18.2	99.5	18.3	35.6	0.0	15.6
	4	20	80	28	0.8	26.6	99.2	26.8	55.7	0.0	24.5
#HR. WA.11	4	20	50	28	3.3	25.6	96.7	26.5	51.8	0.5	23.0
	4	20	80	28	5.2	26.9	94.8	28.4	69.2	0.0	30.4
#HR. WA.15	4	20	80	28	0.6	24.7	99.4	24.8	56.0	1.0	25.1
#HR. WA.16	4	20	80	28	0.7	17.7	99.3	17.8	40.6	0.8	18.2
#HR. SSA.1	4	20	80	28	1.7	16.9	98.3	17.1	10.4	0.8	4.9
	4	40	80	7	1.6	15.8	98.5	16.1	9.5	1.0	4.7
	4	40	80	14	1.7	15.4	98.3	15.7	9.9	0.8	4.7
	20	40	80	3	1.8	11.1	98.2	11.3	9.0	0.8	4.3
#HR. SSA.2	4	20	80	28	0.7	5.6	99.3	5.7	7.0	0.8	3.4
#HR. SSA.3	4	20	80	28	0.6	2.4	99.4	2.4	2.0	0.0	0.9
#HR. SSA.4	4	20	80	28	0.9	2.7	99.2	2.7	1.7	0.3	0.9

2.3. Denmark

MSWI ashes and sewage sludge ashes from Denmark did not show a high CO₂ sequestration potential, with the highest value of 5.9 wt% CO₂ for #DK.MSWI-FA.1.

Table 3: TGA and calcimetric measurements for MSWI ashes and SSA from Denmark.

Sample ID	CO ₂ conc. (%)	T (°C)	RH (%)	Time (days)	TGA (weight losses-%)		Calculations (TGA)		Calculations (calimeter)		
					0-150 °C	550-950 °C	% dry matter	% CO ₂ /dry matter	% CaCO ₃	% Dolomite	% CO ₂
#DK.MSWI-FA.1	4	20	80	28	1.5	13.3	98.5	13.5	12.6	0.8	5.9
	4	40	80	7	1.8	11.8	98.2	12.0	10.8	1.6	5.5
	4	40	80	14	1.6	11.5	98.4	11.7	11.6	1.2	5.6
	20	40	80	3	1.8	14.3	98.2	14.5	12.0	1.2	5.8
#DK.SSA-FA.1	4	20	80	28	0.3	0.5	99.7	0.5	0.6	0.0	0.2
#DK.SSA-FA.2	4	20	80	28	0.2	0.8	99.8	0.8	0.8	0.0	0.4
#DK.MSWI-FA.2	4	20	80	28	0.4	4.9	99.6	4.9	7.8	1.0	3.9
	4	40	80	7	0.9	9.2	99.1	9.3	6.6	1.7	3.7
	4	40	80	14	1.0	8.1	99.0	8.2	8.4	1.0	4.2
#DK.MSWI-FA.3	4	20	80	28	0.6	2.7	99.4	2.7	3.9	0.3	1.8
#DK.MSWI-FA.4	4	20	80	28	0.5	3.1	99.5	3.1	3.4	0.5	1.7

2.4. Finland

The highest CO₂ content (11.6 wt%) of the ashes from Finland was found in the co-combustion ash (#FI.CC.APC.8), while other ashes showed a lower potential for CO₂ sequestration.

Table 4: TGA and calcimetric measurements for co-combustion ashes from Finland.

Sample ID	CO ₂ conc. (%)	T (°C)	RH (%)	Time (days)	TGA (weight losses-%)		Calculations (TGA)		Calculations (calcimetric)		
					0-150 °C	550-950 °C	% dry matter	% CO ₂ /dry matter	% CaCO ₃	% Dolomite	% CO ₂
#FI.CC.APC.8	4	20	80	28	10.2	13.8	89.9	15.4	26.3	0.0	11.6
	4	40	80	7	9.1	13.8	90.9	15.2	24.1	1.4	11.3
	4	40	80	14	9.2	14.2	90.8	15.6	25.2	0.7	11.4
	20	40	80	3	7.7	13.2	92.3	14.3	25.7	0.7	11.6
#FI.CC.FA.8	4	20	80	28	0.7	5.2	99.3	5.2	9.2	1.6	4.8
	4	40	80	7	0.7	4.9	99.3	4.9	8.0	2.0	4.5
	4	40	80	14	0.8	4.7	99.2	4.7	8.2	1.9	4.5
#FI.CC.BA.8	4	20	80	28	0.0	0.5	100.0	0.5	0.8	0.0	0.4

2.5. The Netherlands

Biomass ashes from the Netherlands showed a high sequestration potential with high CO₂ content: 17.2 wt% for #NL.B.FA.1 and 17.3 wt% for #NL.WA.FA.4.

Table 5: TGA and calcimetric measurements for biomass ashes from the Netherlands.

Sample ID	CO ₂ conc. (%)	T (°C)	RH (%)	Time (days)	TGA (weight losses-%)		Calculations (TGA)		Calculations (calcimetric)		
					0-150 °C	550-950 °C	% dry matter	% CO ₂ /dry matter	% CaCO ₃	% Dolomite	% CO ₂
#NL.B.FA.1	4	20	80	28	2.1	20.8	97.9	21.2	37.8	1.3	17.2
	4	40	80	7	1.9	19.6	98.1	20.0	36.2	1.3	16.5
	4	40	80	14	1.5	19.9	98.5	20.2	36.3	1.2	16.5
	20	40	80	3	1.9	19.6	98.2	19.9	36.5	1.1	16.5
#NL.B.FA.2	4	20	80	28	1.0	6.9	99.0	7.0	14.0	1.0	6.7
	4	40	80	7	0.5	5.9	99.5	5.9	11.7	1.2	5.7
	4	40	80	14	0.9	6.2	99.1	6.3	13.0	0.9	6.2
#NL.WA.FA.4	4	20	80	28.0	1.4	29.5	98.6	29.9	38.1	0.5	17.0
	4	40	80	7.0	1.1	27.2	98.9	27.5	37.8	1.2	17.2
	4	40	80	14.0	1.7	29.2	98.3	29.7	38.3	1.0	17.3

2.6. Belgium

Tables 6 and 7 show the TGA and calcimetric measurements for the ashes from Belgium: from the company Orbix and University of Ghent. The highest sequestration potential was determined for the MSWI ash (#BE.MSWI-FA.IV4).

Table 6: TGA and calcimetric measurements for the ashes received from Orbix.

Sample ID	CO ₂ conc. (%)	T (°C)	RH (%)	Time (days)	TGA (weight losses-%)		Calculations (TGA)		Calculations (calcimetric)		
					0-150 °C	550-950 °C	% dry matter	% CO ₂ /dry matter	% CaCO ₃	% Dolomite	% CO ₂
#BE.ORB. 1	4	40	80	7	1.3	9.0	98.7	9.1	17.7	8.3	11.8
	4	40	80	14	1.5	9.5	98.5	9.7	20.7	5.8	11.9
#BE.ORB. 2	4	40	80	7	1.1	5.5	98.9	5.6	8.9	5.0	6.3
	4	40	80	14	1.2	6.1	98.8	6.2	10.2	3.6	6.2
#BE.ORB. 3	4	40	80	7	1.2	6.3	98.8	6.4	17.1	1.3	8.1
	4	40	80	14	1.1	6.5	98.9	6.5	18.5	1.3	8.7

Table 7: TGA and calcimetric measurements for co-combustion and MSWI ashes from Belgium.

Sample ID	CO ₂ conc. (%)	T (°C)	RH (%)	Time (days)	TGA (weight losses-%)		Calculations (TGA)		Calculations (calcimetric)		
					0-150 °C	550-950 °C	% dry matter	% CO ₂ /dry matter	% CaCO ₃	% Dolomite	% CO ₂
#BE.CC-FA.SL3	4	40	80	7	2.9	5.4	97.1	5.6	12.2	0.7	5.7
	4	40	80	14	3.0	5.2	97.0	5.4	12.6	1.0	6.0
#BE.CC.BA.SL-VAL3	4	40	80	7	1.1	5.9	98.9	6.0	15.8	0.5	7.1
	4	40	80	14	1.1	5.9	98.9	5.9	15.9	0.7	7.3
#BE.MSW I-BA.IV-VAL3	4	40	80	7	2.7	7.4	97.3	7.6	20.2	1.3	9.5
	4	40	80	14	2.4	7.2	97.6	7.4	20.6	1.1	9.6
#BE.MSW I-FA.IV4	4	40	80	7	2.2	16.2	97.8	16.6	34.0	3.9	16.8
	4	40	80	14	2.1	16.0	97.9	16.3	35.6	3.5	17.3

3. RESULTS FOR LCA

Table 8 contains data on the maximum CO₂ sequestration capacity for all ashes, expressed in g/kg, so that they can be used for further LCA calculations.

Table 8: Maximum CO₂ sequestration capacity for each analyzed ash.

Country	Sample ID	Maximum CO ₂ sequestration capacity (g/kg)
Slovenia	#SI.WA.FA.1	160
	#SI.WA.BA.1	302
	#SI.CC.FA.2	103
	#SI.CC.MA.2	276
	#SI.CC.FA.3	97
	#SI.CC.BA.3	159
	#SI.CC.FA.4	98
	#SI.CC.BA.4	202
Croatia	#HR.WA.1	221
	#HR.WA.2	272
	#HR.WA.3	198
	#HR.WA.4	271
	#HR.WA.6	172
	#HR.WA.7	84
	#HR.WA.8	246
	#HR.WA.9	245
	#HR.WA.11	304
	#HR.WA.15	251
	#HR.WA.16	182
	#HR.SSA.1	49
	#HR.SSA.2	34
	#HR.SSA.3	9
	#HR.SSA.4	9
Denmark	#DK.MSWI-FA.1	59
	#DK.SSA-FA.1	2
	#DK.SSA-FA.2	4
	#DK.MSWI-FA.2	42
	#DK.MSWI-FA.3	18
	#DK.MSWI-FA.4	17
Finland	#FI.CC.APC.8	114
	#FI.CC.FA.8	45
	#FI.CC.BA.8	4
The Netherlands	#NL.B.FA.1	172
	#NL.B.FA.2	67
	#NL.WA.FA.4	173
Belgium	#BE.ORB.1	119
	#BE.ORB.2	62
	#BE.ORB.3	87
	#BE.CC-FA.SL3	60
	#BE.CC.BA.SL-VAL3	73
	#BE.MSWI-BA.IV-VAL3	96
	#BE.MSWI-FA.IV4	173

4. SUMMARY AND CONCLUSIONS

The ashes were selected from various partners from different countries. In total, the selection included 16 wood ashes, 11 co-combustion ashes, 6 sewage sludge ashes, 6 MSWI ashes and 3 others. During this task we were able to establish the methodology to assess the sequestration potential of waste ashes. This methodology includes:

- Sampling (homogenized by quartening)
- Grinding and sieving (below 125 µm)
- Exposure of the ash to accelerated carbonation
- Analysis with a pressure calcimeter and thermogravimetric analysis.

Based on calculations, the amount of CO₂ was quantified using the calcimetric method, since other phases can also be detected with TGA in the temperature range from 550 to 950 °C. We identified the ashes with the highest sequestration potential of about 300 g/kg (#SI.WA.BA.1 and #HR.WA.11) and prepared the data for all ashes for further LCA calculations.

References

- [1] F. Pacheco-Torgal. "Introduction to carbon dioxide sequestration-based cementitious construction materials." in *Carbon Dioxide Sequestration in Cementitious Construction Materials*. vol. 2. no. 1. Elsevier Ltd. 2018. pp. 3–12. doi: 10.1016/B978-0-08-102444-7.00001-0.
- [2] A. Alturki. "The Global Carbon Footprint and How New Carbon Mineralization Technologies Can Be Used to Reduce CO₂ Emissions." *ChemEngineering*. vol. 6. no. 3. 2022. doi: 10.3390/chemengineering6030044.
- [3] D. Y. C. Leung. G. Caramanna. and M. M. Maroto-Valer. "An overview of current status of carbon dioxide capture and storage technologies." *Renew. Sustain. Energy Rev.*. vol. 39. pp. 426–443. 2014. doi: 10.1016/j.rser.2014.07.093.
- [4] R. A. Betts. C. D. Jones. J. R. Knight. R. F. Keeling. and J. J. Kennedy. "El Nino and a record CO₂ rise." *Nat. Clim. Chang.*. vol. 6. pp. 806–810. 2016. [Online]. Available: <http://dx.doi.org/10.1038/nclimate3063>
- [5] "Carbon Dioxide | Vital Signs – Climate Change: Vital Signs of the Planet." <https://climate.nasa.gov/vital-signs/carbon-dioxide/>
- [6] S. K. Kaliyavaradhan and T.-C. Ling. "Potential of CO₂ sequestration through construction and demolition (C & D) waste — An overview." *J. CO₂ Util.*. vol. 20. pp. 234–242. 2017. doi: 10.1016/j.jcou.2017.05.014.
- [7] H. C. Gomes. E. D. Reis. R. C. de Azevedo. C. de S. Rodrigues. and F. S. J. Poggiali. "Carbonation of Aggregates from Construction and Demolition Waste Applied to Concrete: A Review." *Buildings*. vol. 13. no. 4. 2023. doi: 10.3390/buildings13041097.
- [8] European Commission. "The European Green Deal." https://commission.europa.eu/strategy-and-policy/priorities-2019-2024/european-green-deal_en
- [9] L. Miu. "Public perceptions of CCUS in Central and Eastern Europe – implications for community engagement." *Balt. Carbon Forum*. vol. 2. pp. 6–7. 2023. doi: 10.21595/bcf.2023.23580.
- [10] R. Koch. G. Sailer. S. Paczkowski. S. Pelz. J. Poetsch. and J. Müller. "Lab-Scale Carbonation of Wood Ash for CO₂ -Sequestration." *Energies*. vol. 14. p. 7371. 2021. doi: doi.org/10.3390/en14217371.
- [11] L. Li and M. Wu. "An overview of utilizing CO₂ for accelerated carbonation treatment in the concrete industry." *J. CO₂ Util.*. vol. 60. no. March. p. 102000. 2022. doi: 10.1016/j.jcou.2022.102000.
- [12] R. K. Saran. V. Arora. and S. Yadav. "CO₂ sequestration by mineral carbonation: A review." *Glob. Nest J.*. vol. 20. no. 3. pp. 497–503. 2018. doi: 10.30955/gnj.002597.
- [13] R. R. Tamilselvi Dananjayan. P. Kandasamy. and R. Andimuthu. "Direct mineral carbonation of coal fly ash for CO₂ sequestration." *J. Clean. Prod.*. vol. 112. pp. 4173–4182. 2016. doi: 10.1016/j.jclepro.2015.05.145.
- [14] M. Ouyang and Y. Cao. "Utilizations of reaction exothermic heat to compensate the cost of the permanent CO₂ sequestration through the geological mineral CO₂ carbonation." *Energy*. vol. 284. no. June. p. 128626. 2023. doi: 10.1016/j.energy.2023.128626.



**Funded by
the European Union**

- [15] N. Lippiatt, T. C. Ling, and S. Y. Pan. "Towards carbon-neutral construction materials: Carbonation of cement-based materials and the future perspective." *J. Build. Eng.*, vol. 28, p. 101062. 2020. doi: 10.1016/j.jobbe.2019.101062.
- [16] W. Ashraf. "Carbonation of cement-based materials: Challenges and opportunities." *Constr. Build. Mater.*, vol. 120, pp. 558–570. 2016. doi: 10.1016/j.conbuildmat.2016.05.080.
- [17] S. O. Ekelu. "A review on effects of curing, sheltering, and CO₂ concentration upon natural carbonation of concrete." *Constr. Build. Mater.*, vol. 127, pp. 306–320. 2016. doi: 10.1016/j.conbuildmat.2016.09.056.
- [18] S. Tominc and V. Ducman. "Methodology for Evaluating the CO₂ Sequestration Capacity of Waste Ashes." *Materials (Basel)*, vol. 16, no. 15. 2023. doi: 10.3390/ma16155284.
- [19] G. Costa, R. Baciocchi, A. Poletti, R. Pomi, C. D. Hills, and P. J. Carey. "Current status and perspectives of accelerated carbonation processes on municipal waste combustion residues." *Environ. Monit. Assess.*, vol. 135, no. 1–3, pp. 55–75. 2007. doi: 10.1007/s10661-007-9704-4.
- [20] S. Y. Nam, J. Seo, T. Thriveni, and J. W. Ahn. "Accelerated carbonation of municipal solid waste incineration bottom ash for CO₂ sequestration." *Geosystem Eng.*, vol. 15, no. 4, pp. 305–311. 2012. doi: 10.1080/12269328.2012.732319.
- [21] M. Zajac, J. Skibsted, F. Bullerjahn, and J. Skocek. "Semi-dry carbonation of recycled concrete paste." *J. CO₂ Util.*, vol. 63, no. June. 2022. doi: 10.1016/j.jcou.2022.102111.
- [22] R. Infante Gomes, C. Brazão Farinha, R. Veiga, J. de Brito, P. Faria, and D. Bastos. "CO₂ sequestration by construction and demolition waste aggregates and effect on mortars and concrete performance - An overview." *Renew. Sustain. Energy Rev.*, vol. 152, no. August. 2021. doi: 10.1016/j.rser.2021.111668.
- [23] M. Quaghebeur, P. Nielsen, L. Horckmans, and D. Van Mechelen. "Accelerated carbonation of steel slag compacts: Development of high-strength construction materials." *Front. Energy Res.*, vol. 3. 2015. doi: 10.3389/fenrg.2015.00052.
- [24] F. Winnefeld, A. Leemann, A. German, and B. Lothenbach. "CO₂ storage in cement and concrete by mineral carbonation." *Curr. Opin. Green Sustain. Chem.*, vol. 38, no. December, p. 100672. 2022. doi: 10.1016/j.cogsc.2022.100672.
- [25] B. Zhan, C. S. Poon, Q. Liu, S. Kou, and C. Shi. "Experimental study on CO₂ curing for enhancement of recycled aggregate properties." *Constr. Build. Mater.*, vol. 67, pp. 3–7. 2014. doi: 10.1016/j.conbuildmat.2013.09.008.
- [26] J. Zhang, C. Shi, Y. Li, X. Pan, C.-S. Poon, and Z. Xie. "Performance Enhancement of Recycled Concrete Aggregates through Carbonation." *J. Mater. Civ. Eng.*, vol. 27, no. 11. 2015. doi: 10.1061/(asce)mt.1943-5533.0001296.
- [27] E. Possan, W. A. Thomaz, G. A. Aleandri, E. F. Felix, and A. C. P. dos Santos. "CO₂ uptake potential due to concrete carbonation: A case study." *Case Stud. Constr. Mater.*, vol. 6, pp. 147–161. 2017. doi: 10.1016/j.cscm.2017.01.007.
- [28] S. M. Shih, C. S. Ho, Y. S. Song, and J. P. Lin. "Kinetics of the reaction of



**Funded by
the European Union**

- Ca(OH)₂ with CO₂ at low temperature." *Ind. Eng. Chem. Res.*, vol. 38, no. 4, pp. 1316–1322, 1999. doi: 10.1021/ie980508z.
- [29] S. Steiner, B. Lothenbach, T. Proske, A. Borgschulte, and F. Winnefeld. "Effect of relative humidity on the carbonation rate of portlandite, calcium silicate hydrates and ettringite." *Cem. Concr. Res.*, vol. 135, p. 106116, 2020. doi: 10.1016/j.cemconres.2020.106116.
- [30] K. O. Kjellsen, M. Guimaraes, and A. Nilsson. "The CO₂ Balance of Concrete in a Life Cycle Perspective." 2005.
- [31] D. N. Padmaraj, D., Arnepalli. "Carbonation in lime-stabilized clays: mechanism, effects, and future prospects.." *Bull Eng Geol Env.*, vol. 258, 2023. doi: <https://doi.org/10.1007/s10064-023-03273-6>.
- [32] Z. Li, H. Sun, and N. Cai. "Rate equation theory for the carbonation reaction of CaO with CO₂." *Energy and Fuels*, vol. 26, no. 7, pp. 4607–4616, 2012. doi: 10.1021/ef300607z.
- [33] S. Abramov *et al.*. "Heavy metal mobility and valuable contents of processed municipal solid waste incineration residues from Southwestern Germany." *Waste Manag.*, vol. 79, pp. 735–743, 2018. doi: 10.1016/j.wasman.2018.08.010.
- [34] S. Tominc, V. Ducman, W. Wisniewski, T. Luukkonen, G. M. Kirkelund, and L. M. Ottosen. "Recovery of Phosphorus and Metals from the Ash of Sewage Sludge, Municipal Solid Waste, or Wood Biomass: A Review and Proposals for Further Use." *Materials (Basel)*, vol. 16, no. 21, 2023. doi: 10.3390/ma16216948.
- [35] N. Tripathi, C. D. Hills, R. S. Singh, and J. S. Singh. "Offsetting anthropogenic carbon emissions from biomass waste and mineralised carbon dioxide." *Sci. Rep.*, vol. 10, no. 1, pp. 1–9, 2020. doi: 10.1038/s41598-020-57801-5.
- [36] "EN 196-2:2013; Method of Testing Cement—Part 2: Chemical Analysis of Cement.." 2013
- [37] R. G. Fernández, C. P. García, A. G. Lavín, and J. L. Bueno De Las Heras. "Study of main combustion characteristics for biomass fuels used in boilers." *Fuel Process. Technol.*, vol. 103, pp. 16–26, 2012. doi: 10.1016/j.fuproc.2011.12.032.

Appendix

The calibration curve for the calcimetric measurements is shown in Figure A1. Based on the chemical and mineralogical composition of the ash it is possible to predict which ash has a sequestration potential. The mean values of the primary oxides measured by XRF and the loss on ignition (LOI) at 950 °C are given in the Tables A1-A7. The XRD analysis enables to monitor the carbonation process and the relative content of e.g. calcite/lime as shown in Figure A2.

Figure A1: Calibration curve for calcimetric measurement

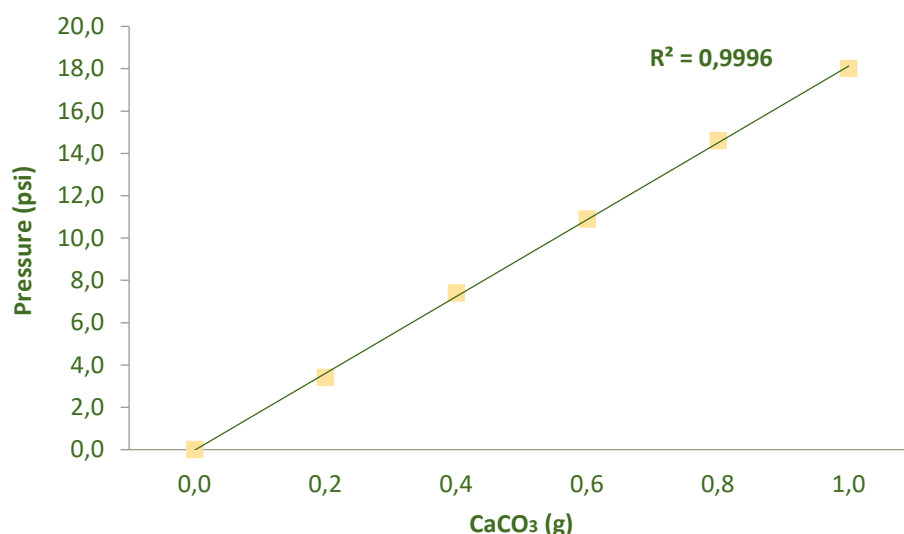


Table A1: XRF results for ashes from Slovenia.

	#SI.WA. FA.1	#SI.WA. BA.1	#SI.CC. FA.2	#SI.CC. MA.2	#SI.CC. FA.3	#SI.CC. BA.3	#SI.CC. FA.4	#SI.CC. BA.4
LOI 950°C	29.91	26.09	11.71	14.55	16.98	12.79	22.31	7.21
Na ₂ O	0.56	0.48	0.74	0.41	0.28	0.57	21.92	2.28
MgO	3.78	5.88	5.99	2.12	8.21	10.25	1.60	3.46
Al ₂ O ₃	5.62	3.35	11.27	11.08	10.87	7.43	6.85	20.05
SiO ₂	19.04	5.64	22.90	14.45	27.78	31.17	8.19	25.91
P ₂ O ₅	2.24	2.82	0.28	0.26	0.56	1.00	0.89	2.45
SO ₃	1.00	0.32	1.70	0.20	1.69	0.07	3.85	0.86
K ₂ O	5.65	8.14	0.99	0.25	2.16	3.21	2.48	0.55
CaO	29.27	44.95	34.01	55.40	19.77	28.98	13.50	28.62
TiO ₂	0.37	0.07	0.73	0.22	0.52	0.32	0.97	1.85
V ₂ O ₅	0.01	0.01	0.02	/	0.02	0.02	0.01	0.03
Cr ₂ O ₃	0.01	0.01	0.02	/	0.01	0.02	0.04	0.11
MnO	0.43	0.93	0.15	0.03	0.27	0.31	0.06	0.21
Fe ₂ O ₃	1.70	0.68	8.53	0.56	10.44	3.56	1.21	3.37
Co ₃ O ₄	/	/	0.01	/	0.02	/	/	/
NiO	0.00	0.01	0.01	/	0.01	0.01	/	0.02
CuO	0.01	0.02	0.04	0.06	0.01	0.01	0.10	0.71
ZnO	0.05	0.09	0.27	0.03	0.04	0.02	1.04	1.02
As ₂ O ₃	0.07	0.08	0.08	0.07	0.08	0.10	0.16	0.17

Rb ₂ O	0.02	0.02	0.01	0.01	0.01	0.01	0.01	0.01
SrO	0.06	0.09	0.08	0.09	0.07	0.05	0.02	0.05
ZrO ₂	0.02	0.00	0.02	0.02	0.02	0.02	0.01	0.05
BaO	0.12	0.29	0.19	0.03	0.17	0.07	0.07	0.23
PbO	0.02	/	0.03	0.02	0.01	0.02	0.09	0.06
Cl	/	/	/	/	/	/	14.45	0.56
SUM	99.96	99.95	99.76	99.85	99.97	99.97	99.85	99.83

Table A2: XRF results for WBA from Croatia.

	#HR. WA.1	#HR. WA.2	#HR. WA.3	#HR. WA.4	#HR. WA.6	#HR. WA.7	#HR. WA.8	#HR. WA.9	#HR. WA.11	#HR. WA.15	#HR. WA.16
LOI 950°C	20.81	20.49	12.54	13.49	7.53	5.17	15.56	11.89	20.99	14.51	8.25
Na ₂ O	0.70	1.99	0.38	0.68	0.64	0.48	0.51	/	0.27	0.68	0.88
MgO	3.05	2.84	3.56	3.12	3.05	4.43	4.72	2.43	5.48	2.69	4.53
Al ₂ O ₃	3.83	0.31	2.75	3.38	6.06	9.14	1.86	1.51	0.96	2.50	3.64
SiO ₂	15.42	1.03	9.22	14.66	20.71	36.61	5.94	6.86	2.67	9.72	12.14
P ₂ O ₅	2.17	2.01	3.68	2.60	3.38	2.30	3.16	1.40	1.99	2.06	4.03
SO ₃	3.44	10.00	0.97	0.50	2.61	0.57	6.66	1.38	5.90	1.24	12.20
K ₂ O	9.82	19.06	4.34	8.13	8.57	8.74	14.15	3.08	18.98	5.54	8.93
CaO	37.51	40.97	59.86	50.71	40.63	25.30	44.79	69.89	41.12	58.18	41.40
TiO ₂	0.33	0.04	0.24	0.22	0.46	0.58	0.16	0.12	0.08	0.18	0.28
Cr ₂ O ₃	0.01	0.02	0.01	0.03	0.04	0.02	0.01	0.01	0.03	0.01	0.02
MnO	0.52	0.23	0.40	0.38	3.20	0.50	0.69	0.28	0.40	0.87	0.67
Fe ₂ O ₃	2.01	0.36	1.66	1.84	2.68	5.95	1.18	0.86	0.64	1.38	1.94
CuO	0.02	0.03	0.03	0.02	0.05	0.01	0.03	0.03	0.04	0.02	0.02
ZnO	0.05	0.04	0.01	/	0.06	0.03	0.10	0.01	0.10	0.03	0.17
SrO	0.09	0.10	0.16	0.13	0.09	0.05	0.11	0.15	0.06	0.12	0.10
BaO	0.13	0.13	0.21	0.13	0.14	0.14	0.22	0.09	0.11	0.30	0.11
Cl	0.12	0.41	0.03	/	0.14	0.01	0.22	0.03	0.24	/	0.73
SUM	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00

Table A3: XRF results for SSA ashes from Croatia.

	#HR.SSA.1	#HR.SSA.2	#HR.SSA.3	#HR.SSA.4
LOI 950°C	19.44	31.84	13.21	13.81
Na ₂ O	0.64	0.80	0.66	1.25
MgO	1.72	2.45	3.05	2.38
Al ₂ O ₃	10.28	6.81	13.60	13.52
SiO ₂	26.90	21.27	38.36	41.45
P ₂ O ₅	10.98	7.12	8.54	6.79
SO ₃	3.71	4.65	2.26	1.63
K ₂ O	1.14	1.34	2.28	1.94
CaO	18.46	17.48	9.65	7.38
TiO ₂	0.55	0.64	0.75	0.72
Cr ₂ O ₃	0.06	0.06	0.05	0.08
MnO	0.09	0.08	0.16	0.24
Fe ₂ O ₃	5.73	4.84	6.89	8.54
CuO	0.03	0.07	0.31	0.03

ZnO	0.13	0.15	0.11	0.03
SrO	0.03	0.02	0.03	0.11
BaO	0.07	0.09	0.09	0.12
Cl	0.07	0.33	0.03	0.03
SUM	100.00	100.00	100.00	100.00

Table A4: XRF results for ashes from Denmark.

	#DK.MSWI-FA.1	#DK.SSA-FA.1	#DK.SSA-FA.2	#DK.MSWI-FA.2	#DK.MSWI-FA.3	#DK.MSWI-FA.4
LOI 950°C	9.55	1.17	1.35	3.58	4.62	7.99
Na ₂ O	3.98	0.96	1.22	5.38	10.14	13.42
MgO	2.76	3.48	4.55	3.36	3.04	2.58
Al ₂ O ₃	10.83	10.49	6.84	9.07	7.28	5.59
SiO ₂	21.07	30.67	26.52	24.31	17.86	14.84
P ₂ O ₅	1.36	22.49	25.98	1.86	1.57	1.38
SO ₃	7.29	0.24	0.12	10.81	10.73	11.23
K ₂ O	3.49	2.01	1.88	2.51	5.45	6.58
CaO	24.87	14.92	14.86	26.14	21.17	17.60
TiO ₂	1.82	0.74	0.80	2.38	1.78	1.48
V ₂ O ₅	0.02	0.02	0.02	0.02	0.02	0.01
Cr ₂ O ₃	0.11	0.01	0.02	0.05	0.03	0.03
MnO	0.11	0.10	0.09	0.19	0.19	0.17
Fe ₂ O ₃	6.24	11.76	14.70	2.09	1.63	1.43
Co ₃ O ₄	0.01	0.01	0.01	/	/	/
NiO	0.02	0.01	0.01	0.01	0.01	0.01
CuO	0.08	0.08	0.10	0.04	0.08	0.11
ZnO	1.92	0.31	0.40	1.31	1.94	2.25
As ₂ O ₃	0.09	0.07	0.09	0.14	0.15	0.10
Rb ₂ O	0.01	0.01	0.01	0.01	0.02	0.02
SrO	0.07	0.26	0.23	0.06	0.05	0.04
ZrO ₂	0.03	0.03	0.02	0.04	0.03	0.02
SnO ₂	0.11	/	/	0.03	0.05	0.07
Sb ₂ O ₃	0.08	/	/	0.05	0.06	0.06
Cs ₂ O	0.01	/	0.01	/	0.02	0.02
BaO	0.15	0.12	0.13	0.36	0.28	0.26
La ₂ O ₃	/	/	0.01	/	/	/
PbO	0.01	0.01	0.01	0.01	/	/
Cl	3.93	/	/	4.16	10.30	12.72
SUM	99.98	99.96	99.96	99.96	99.96	99.99

Table A5: XRF results for ashes from Finland.

	#FI.CC.APC.8	#FI.CC.FA.8	#FI.CC.BA.8
LOI 950°C	16.30	2.79	0.06
Na ₂ O	1.53	3.74	3.65
MgO	2.49	3.85	2.32
Al ₂ O ₃	8.51	14.97	11.57
SiO ₂	15.57	31.11	62.62
P ₂ O ₅	1.38	2.50	0.80

SO ₃	9.11	6.10	0.17
K ₂ O	0.94	2.70	2.79
CaO	32.13	19.40	10.32
TiO ₂	0.52	1.37	0.69
V ₂ O ₅	0.02	0.03	0.02
Cr ₂ O ₃	0.03	0.08	0.11
MnO	0.30	0.52	0.29
Fe ₂ O ₃	6.45	9.65	3.63
Co ₃ O ₄	0.01	0.01	/
NiO	0.01	0.02	0.01
CuO	0.01	0.16	0.19
ZnO	0.09	0.25	0.31
As ₂ O ₃	0.08	0.12	0.10
Rb ₂ O	0.01	0.02	0.01
SrO	0.04	0.08	0.06
ZrO ₂	0.01	0.03	0.06
BaO	0.08	0.19	0.21
La ₂ O ₃	/	0.02	0.01
Cl	4.38	0.31	/
PbO	/	/	0.01
SUM	99.96	99.96	99.99

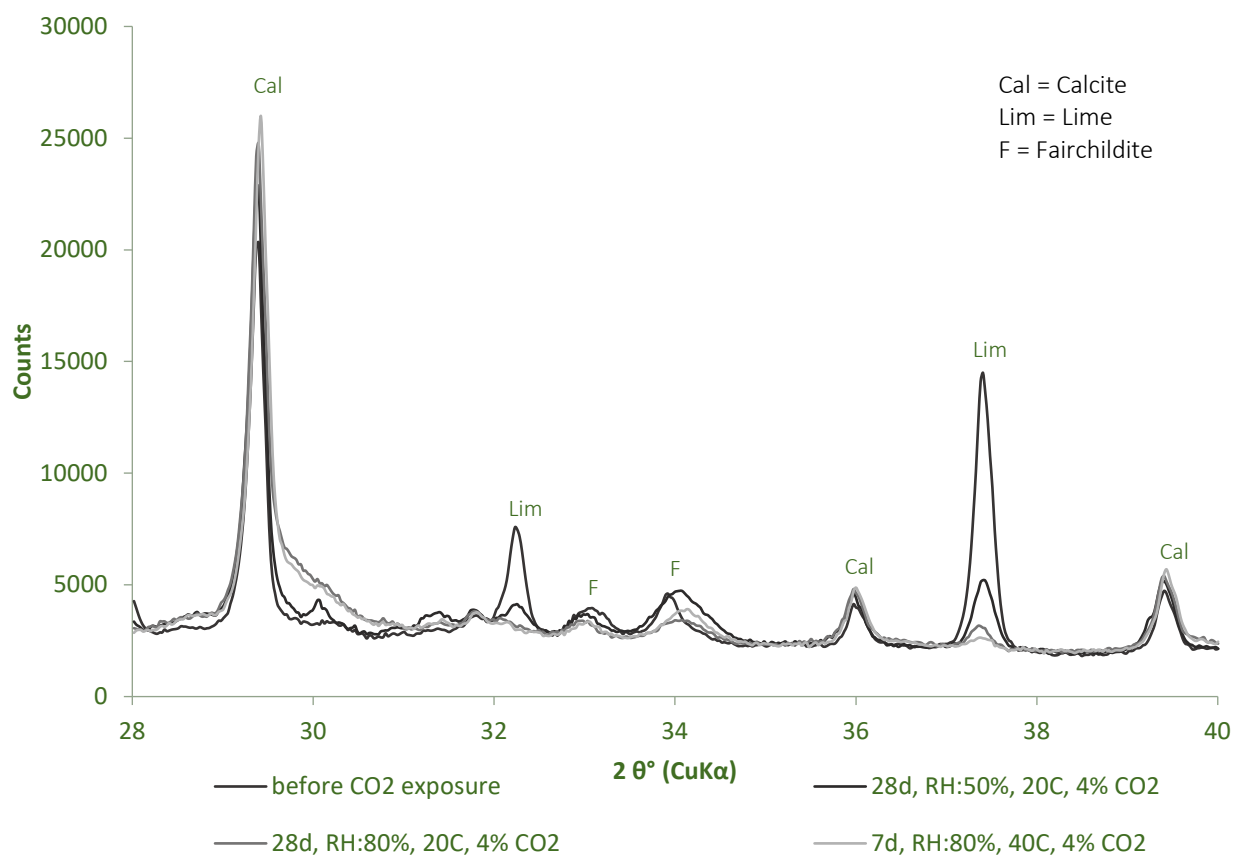
Table A6: XRF results for ashes from The Netherlands.

	#NL.B.FA.1	#NL.B.FA.2	#NL.WA.FA.4
LOI 950°C	13.85	3.94	19.90
Na ₂ O	1.48	1.90	2.95
MgO	3.17	3.67	2.42
Al ₂ O ₃	5.63	7.54	3.69
SiO ₂	25.51	45.20	14.80
P ₂ O ₅	2.58	2.08	0.95
SO ₃	3.88	1.62	5.86
K ₂ O	4.68	1.75	1.98
CaO	33.38	22.25	36.63
TiO ₂	1.48	4.10	1.43
V ₂ O ₅	0.01	0.03	0.01
Cr ₂ O ₃	0.04	0.11	0.07
MnO	0.27	0.45	0.28
Fe ₂ O ₃	1.86	3.45	1.59
Co ₃ O ₄	/	0.01	/
NiO	0.01	0.02	/
CuO	0.03	0.08	0.04
ZnO	0.49	0.62	3.25
As ₂ O ₃	0.08	0.10	0.09
Rb ₂ O	0.01	0.01	0.00
SrO	0.09	0.09	0.07
ZrO ₂	0.03	0.08	0.02
Cs ₂ O	/	/	0.03

BaO	0.19	0.72	0.22
SnO ₂	/	/	/
Ta ₂ O ₅	0.01	/	/
PbO	0.12	0.10	0.07
Cl	1.10	0.07	3.63
SUM	99.97	99.96	99.96

Table A7: XRF results for ashes from Belgium.

	#BE.ORB.1	#BE.ORB.2	#BE.ORB.3	#BE.CC-FA.SL3	#BE.CC. BA.SL-VAL3	#BE.MSWI-BA. IV-VAL3	#BE.MSWI-FA. IV4
LOI 950°C	4.75	3.78	3.30	8.65	11.93	21.73	9.61
Na ₂ O	3.15	3.78	0.24	1.71	2.27	2.57	2.06
MgO	3.29	3.95	12.92	3.17	1.87	2.70	4.11
Al ₂ O ₃	10.97	3.38	8.66	10.43	10.19	8.80	10.98
SiO ₂	39.02	9.69	26.93	31.09	52.73	32.12	16.12
P ₂ O ₅	2.78	32.10	/	2.79	0.24	1.55	3.58
SO ₃	3.33	2.35	0.24	8.50	1.20	1.43	6.44
K ₂ O	1.46	9.46	/	0.99	1.39	0.72	0.74
CaO	24.79	2.39	42.10	24.89	13.10	20.29	38.10
TiO ₂	2.23	25.71	1.03	1.40	0.49	0.86	2.87
V ₂ O ₅	0.02	2.35	0.07	0.03	0.01	0.01	0.02
Cr ₂ O ₃	0.10	0.02	2.33	0.04	0.04	0.06	0.12
MnO	0.10	0.12	1.07	0.10	0.12	0.23	0.12
Fe ₂ O ₃	2.54	0.11	0.76	4.91	3.84	5.59	1.88
Co ₃ O ₄	0.00	2.49	/	0.00	/	0.01	0.01
NiO	0.09	/	0.08	0.01	0.01	0.02	0.01
CuO	0.04	0.08	/	0.08	0.08	0.19	0.01
ZnO	0.43	0.05	0.00	0.50	0.11	0.69	0.53
As ₂ O ₃	0.06	1.10	0.06	0.12	0.12	0.10	0.11
Rb ₂ O	0.00	0.08	0.00	0.01	0.01	0.01	0.01
SrO	0.07	0.01	0.03	0.12	0.03	0.07	0.08
ZrO ₂	0.04	0.08	0.03	0.05	0.09	0.03	0.04
Cs ₂ O	/	0.08	/	/	/	0.01	/
BaO	0.18	/	/	0.27	0.09	0.14	0.17
SnO ₂	/	0.18	/	0.01	/	0.01	0.01
Nb ₂ O ₅	0.00	0.02	0.14	/	0.00	0.01	/
PbO	0.00	0.00	/	/	0.02	0.03	/
Cl	0.56	/	/	0.07	/	/	2.23
PtO ₂	/	/	/	0.02	0.01	0.01	/
Au	/	/	/	0.01	0.01	0.01	0.00
SUM	99.99	99.99	99.99	99.98	99.99	99.97	99.94

Figure A2: X-ray diffraction patterns of selected sample #SI.WA.BA.1.



**Funded by
the European Union**